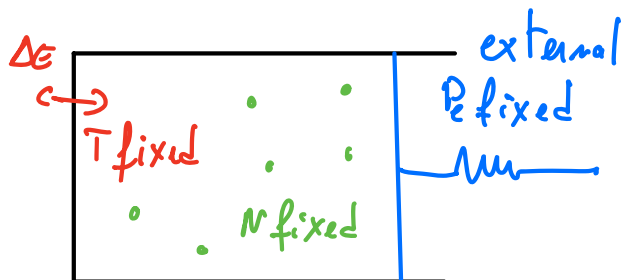


4.3) liquid gas phase transition in the isobaric ensemble

(1)

By changing ensemble, we show that

$$P(\varphi) = \frac{1}{Z_I} e^{-\beta E(\varphi) - \beta P_e V(\varphi)}$$



$$\text{when } Z_I(P, T, N) = \int_0^\infty dV e^{-\beta P_e V} Z_c(V, T, N) = \int_0^\infty dV e^{-\beta [P_e V + F(T, V, N)]}$$

At large N , F is extensive, $F(N, V, T) \simeq N f(v, T)$; $v = \frac{V}{N}$ so that

$$Z_I = \int_0^\infty N dv e^{-\beta N [P_e v + f(v, T)]} = N \int_0^\infty dv e^{-\beta N \mu_c(v; T, P_e)}$$

when we call $\mu_c(v; T, P_e)$ the Landau chemical potential of the macrostate

with Volume V / free volume $v = \frac{V}{N}$: $\mu_c(v, T, P_e) = P_e v + f(v, T)$

$$\text{As } N \rightarrow \infty, Z_I \sim e^{-\beta N \mu_c(v^*, T, P_e)} = e^{-\beta N [P_e v^* + f(v^*, T)]} = e^{-\beta [P_e v^* + F(v^*, N, T)]}$$

As usual, $P(v) \sim \delta(v - v^*)$ with $v^* = \underset{N \rightarrow \infty}{\text{argmin}} \mu_c(v; T, P_e) = \underset{N \rightarrow \infty}{\text{argmin}} [P_e v + f(v, T)]$

$$\Rightarrow \underset{\text{P}_{\text{external (imposed)}}}{P_e} = - \left. \frac{\partial f}{\partial v} \right|_{v^*} = - \left. \frac{\partial F}{\partial V} \right|_{v^*} = \underset{\text{P}_{\text{canonical (selected)}}}{P_c} \quad \text{if there is a unique solution.}$$

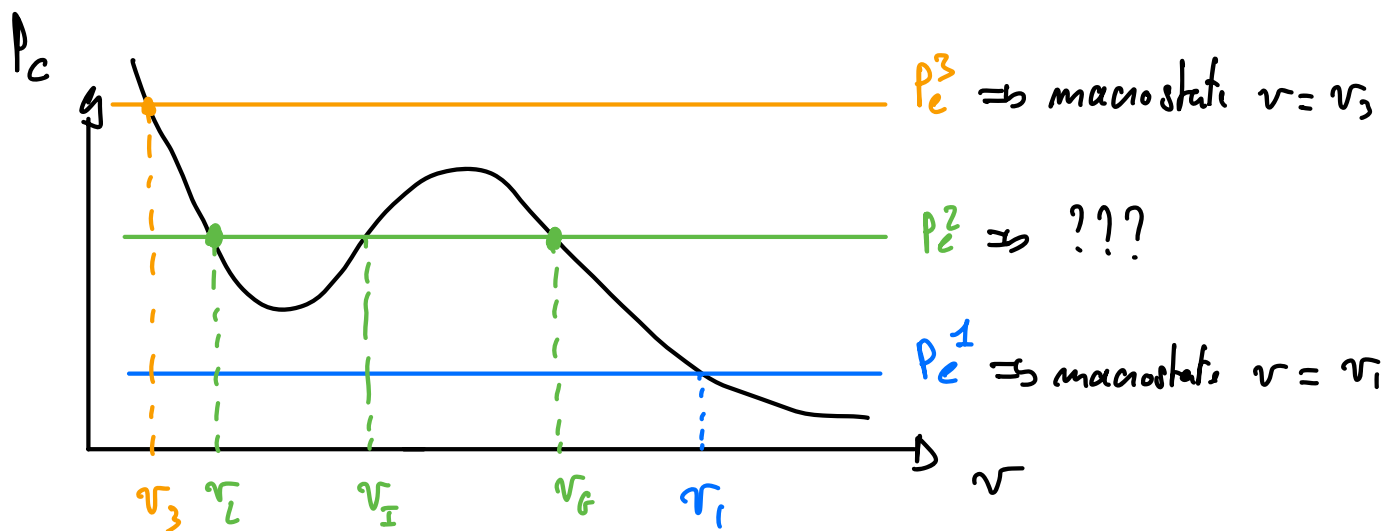
The most likely macrostate is the one whose canonical pressure is equal to the external pressure. Then

$$N \mu_c(v^*) = P_e v^* + F \underset{N \rightarrow \infty}{=} F - G = F - (F - \mu N) = \mu N$$

②

\Rightarrow the chemical potential is the Landau chemical of the most likely macrostate.

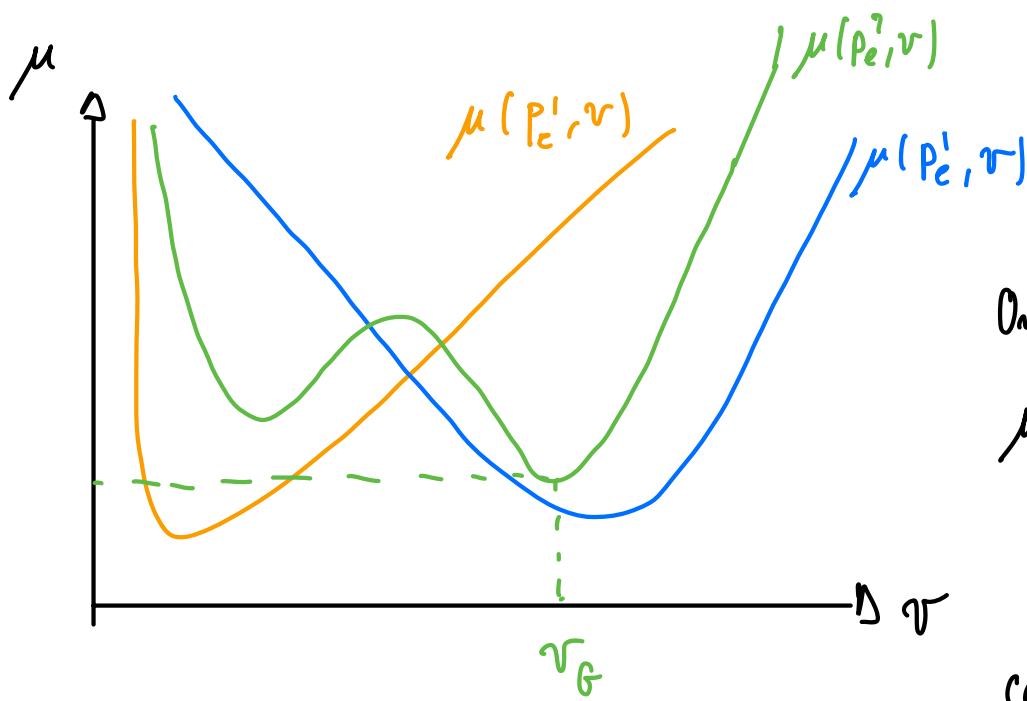
Summary: If we impose an external pressure p_e & there is a unique solution $P_c(v) = p_e$, then we observe a homogeneous phase at free volume $v \Rightarrow$ scenario for $T > T_c$. Q: What about $T < T_c$?



Find $\text{argmin}_v [p_e v + f(v, T)]$

$$Z = \frac{1}{N! \Lambda^{3N}} e^{\beta \frac{N^2 \epsilon}{2v}} \left(v - \frac{N \Omega}{2} \right)^N \Rightarrow f = C^{\text{st}} - \frac{\epsilon}{2v} - kT \ln \left(v - \frac{\Omega}{2} \right)$$

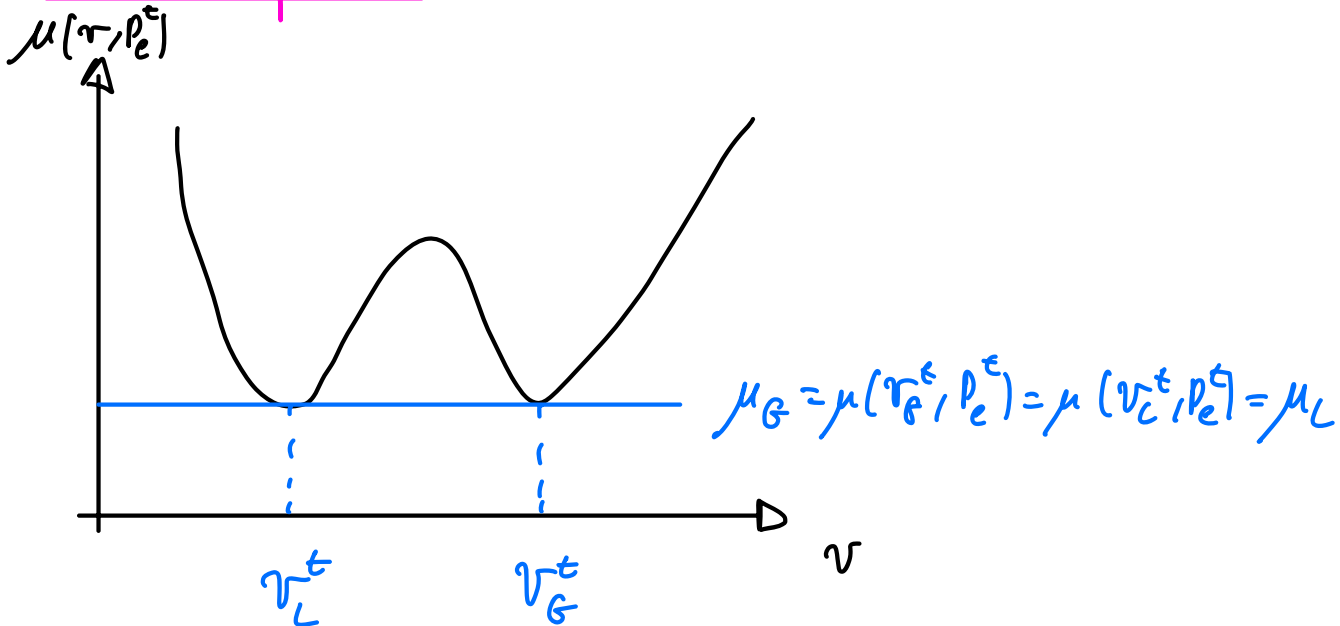
$$\mu = p v + f = \mu_0 + p v - \frac{\epsilon}{2v} - kT \ln \left(v - \frac{\Omega}{2} \right)$$



On this example,
 $\mu(P_e^2, v_G) < \mu(P_e^2, v_L)$
 $\Rightarrow v_G$ wins &
 we observe the
 corresponding macrostate.

Large $P \Rightarrow$ small v win
 Small $P \Rightarrow$ large v win } how do we transition?

Transition pressure



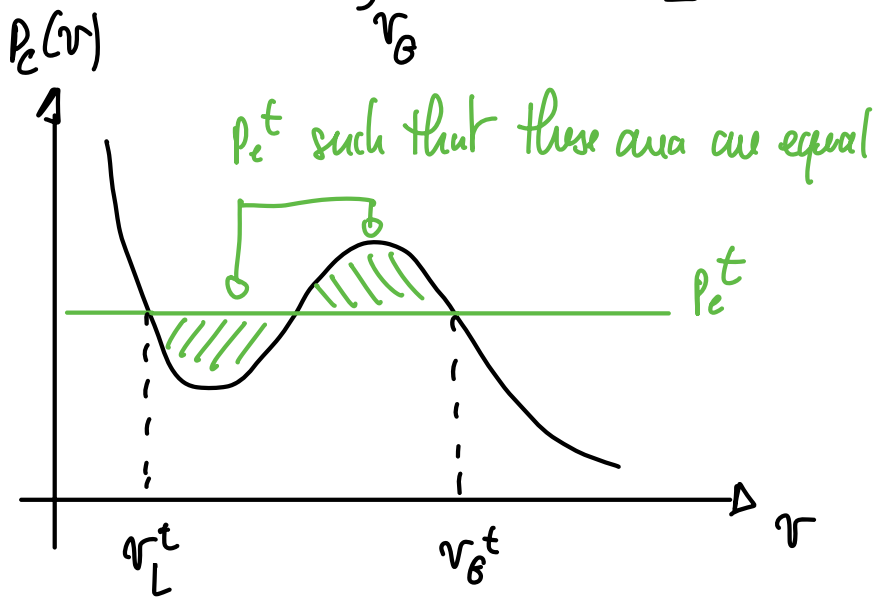
As P_e crosses through P_e^t , the system jumps from v_G^t to v_L^t

How do we find P_c ?

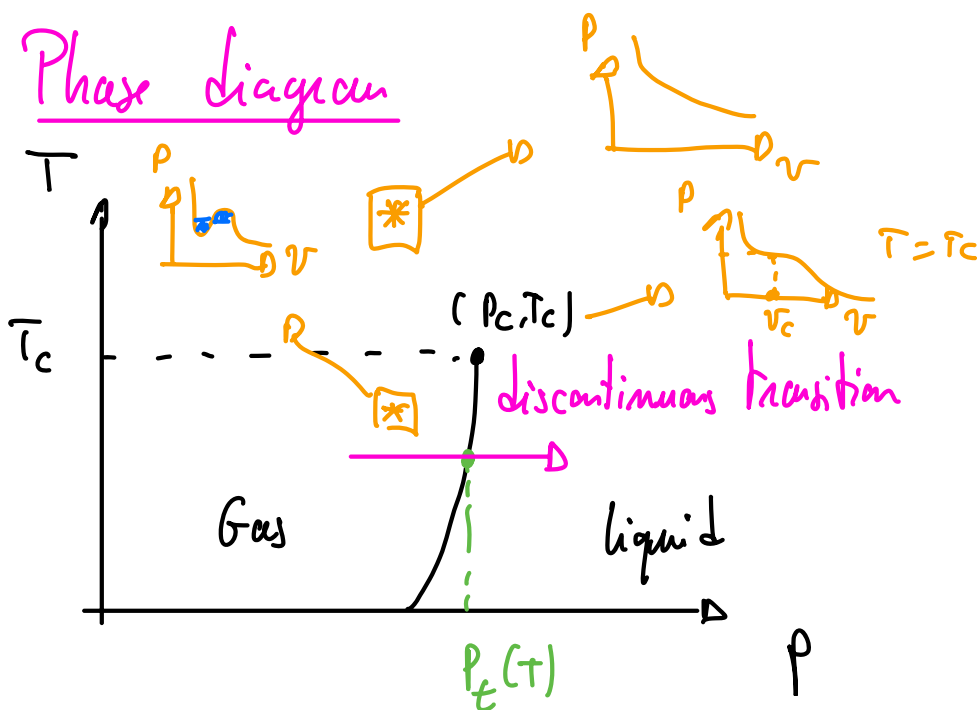
$$\mu(r_g) = \mu(r_c) \Rightarrow \mu(r_g) - \mu(r_c) = \int_{r_g}^{r_c} \frac{d\mu}{dr} dr = 0$$

$$P_c^t + \frac{\partial f}{\partial r} = P_c^t - P_c(r)$$

$$\Rightarrow \int_{r_g}^{r_c} dr [P_c^t - P_c(r)] = 0 \Rightarrow \text{Max well construction}$$



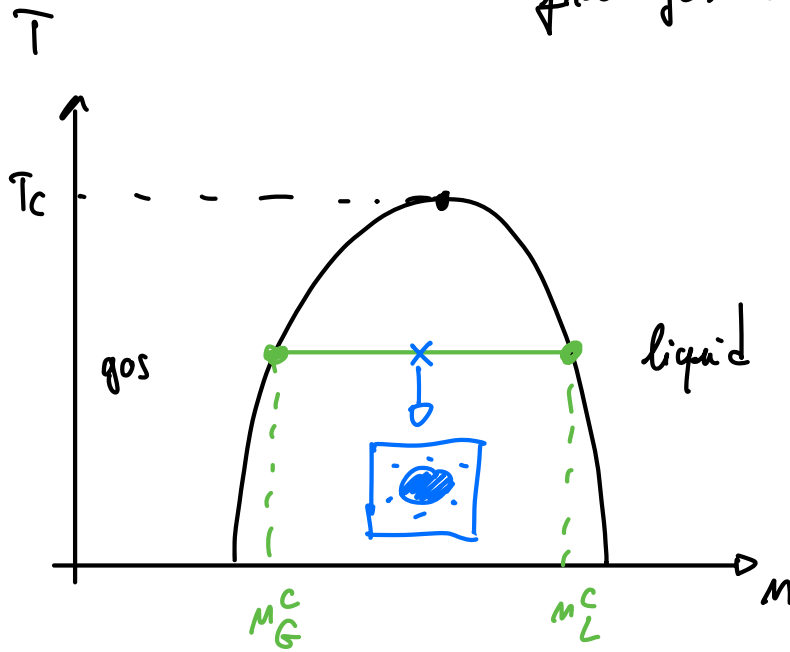
Phase diagram



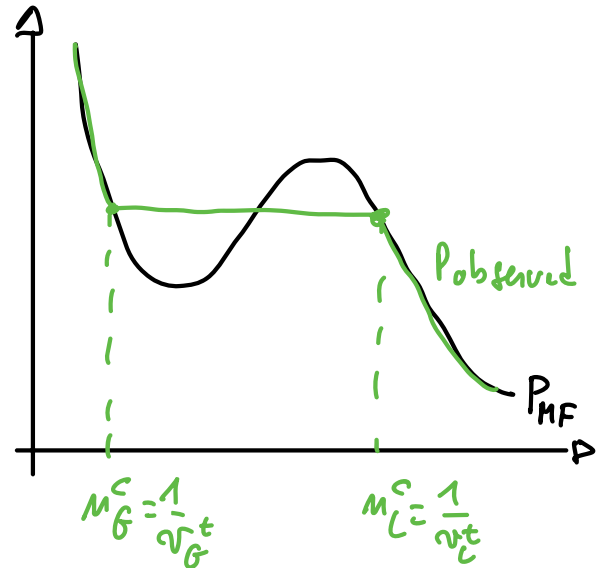
Canonical ensemble

In the canonical ensemble, the system goes from gas to liquid through phase coexistence

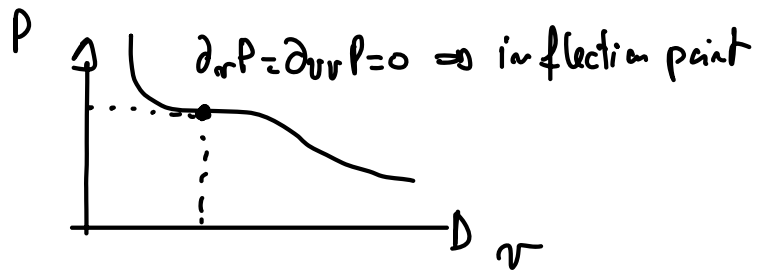
5



Between the gas & the liquid phase, pressure & chemical potential remain constant



4.4) Universality



Let us look at the behaviour close to P_c, T_c, μ_c

$$P(v) = P(v_c) + \left. \frac{\partial P}{\partial v} \right|_{T_c} (v - v_c) + \frac{1}{2} \left. \frac{\partial^2 P}{\partial v^2} \right|_{T_c} (v - v_c)^2 + \frac{1}{6} \left. \frac{\partial^3 P}{\partial v^3} \right|_{T_c} (v - v_c)^3 + \dots \quad (\Delta)$$

$$\text{At } T_c, v_c, \frac{\partial P}{\partial v} = \frac{\partial^2 P}{\partial v^2} = 0$$

(6)

Mean-field

$$p = \frac{h_B T}{v - \frac{\Omega}{2}} - \frac{\epsilon}{2 v^2}$$

$$p'(v) = 0 \Leftrightarrow -\frac{h_B T}{(v - \frac{\Omega}{2})^2} + \frac{\epsilon}{v^3} = 0 \Leftrightarrow \frac{v_c^3}{\epsilon} = \frac{(v_c - \frac{\Omega}{2})^2}{h_B T} \quad (*)$$

$$p''(v) = 0 \quad \frac{2 h_B T}{(v_c - \frac{\Omega}{2})^3} - \frac{3 \epsilon}{v_c^4} = 0 \Leftrightarrow \frac{v_c^4}{3 \epsilon} = \frac{(v_c - \frac{\Omega}{2})^3}{2 h_B T} \quad (**)$$

$$(*) \Rightarrow \frac{v_c}{3} = \frac{v_c}{2} - \frac{\Omega}{4} \Rightarrow v_c = \frac{3\Omega}{2}$$

$$(*) \Rightarrow h_B T_c = \Omega^2 \cdot \epsilon \cdot \frac{8}{27 \Omega^3} = \frac{8 \epsilon}{27 \Omega}$$

$$p_c = \frac{h_B T_c}{v_c - \frac{\Omega}{2}} - \frac{\epsilon}{2 v_c^2} = \frac{2 \epsilon}{27 \Omega^2}$$

Critical point:

Mean-field theory: v_c, T_c, p_c are 3 observables that depend on 2 parameters, μ & Ω
 \Rightarrow 1 dimensionless number

$$\frac{p_c v_c}{h_B T_c} = \frac{3}{8} \Rightarrow \text{parameter free!} \Rightarrow \text{should be the same for all liquid gas phase separation}$$

Experiments: Many systems lead to $\frac{p_c v_c}{h_B T_c} \in [0.28, 0.33]$

\Rightarrow not universal but quite close.

Critical isotherm:

Mean-field theory: At $T = T_c$, $p - p_c \propto (v - v_c)^3$

Experiments $p - p_c \propto (v - v_c)^\delta$ with $\delta \simeq 5.0$ for all simple fluids \Rightarrow universal!

Compressibility: $\kappa = -\frac{1}{v} \frac{\partial v}{\partial p}$

Mean field: $p'(v) \Big|_{v_c} = \frac{8\mu}{27v^3} - \frac{4aT}{v^2} = \frac{4a(T_c - T)}{v} \Rightarrow \kappa \propto \frac{1}{T - T_c} \xrightarrow{T \rightarrow T_c} \infty$

Experiments: $\kappa \propto \frac{1}{|T - T_c|^{1.24}}$ for all simple fluids \Rightarrow universal!

Three surprises

- (i) Some observables are universal, behaving in the exact same way across a range of systems despite their microscopic differences
- (ii) These universal behaviours are not quantitatively predicted by mean-field
- (iii) The universal exponents are not simple numbers ($1, 1/2, \dots$)

Why? Because fluctuations are important. $g(r) \approx g_0$ is a brutal approximation, that fails close to the critical point.

Can we predict all this? Yes! Statistical field theory & 8.334.